#### (19) World Intellectual Property Organization International Bureau



# 

### (43) International Publication Date 9 January 2003 (09.01.2003)

## (10) International Publication Number WO 03/002785 A1

- (51) International Patent Classification7: C22B 34/12
- C25C 3/28.
- (21) International Application Number: PCT/AU02/00843
- (22) International Filing Date: 28 June 2002 (28.06.2002)
- (25) Filing Language: English
- English (26) Publication Language:
- (30) Priority Data:

PR 6029 29 June 2001 (29.06.2001) AU

- (71) Applicant (for all designated States except US): BHP BIL-LITON INNOVATION PTY LTD [AU/AU]; Level 45, 600 Bourke Street, Melbourne, Victoria 3000 (AU).
- (72) Inventors; and
- (75) Inventors/Applicants (for US only): STREZOV, Les [AU/AU]; 7 Marin Street, Adamstown, New South Wales 2289 (AU). RATCHEV, Ivan [AU/AU]; 2 Young Street, Georgetown, New South Wales 2298 (AU). OSBORN, Steve [AU/AU]; 15 Robertson Road, Valentine, New South Wales 2280 (AU).

- (74) Agent: GRIFFITH HACK; 509 St Kilda Road, Melbourne, VIC 3004 (AU).
- (81) Designated States (national): AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NO, NZ, OM, PH, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ, VN, YU, ZA, ZM, ZW.
- (84) Designated States (regional): ARIPO patent (GH, GM, KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZM, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, TR), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG).

#### Published:

with international search report

For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

(54) Title: REDUCTION OF METAL OXIDES IN AN ELECTROLYTIC CELL

(57) Abstract: A method of reducing a titanium oxide in a solid state in an electrolytic cell which includes an anode, a cathode formed at least in part from the titanium oxide, and a molten electrolyte which includes cations of a metal that is capable of chemically reducing the cathode titanium oxide, wich method includes operating the cell at a potential that is above a potential at which cations of the metal that is capable of chemically reducing the cathode titanium oxide deposit as the metal on the cathod, whereby the metal chemically reduces the cathode titanium oxide, and which method is characterised by refreshing the electrolyte and/or changing the cell potential in later stages of the operation of the cell as required having regard to the reactions occurring in the cell and the concentration of oxygen in the titanium oxide in the cell in order to produce high purity titanium.

- 1 -

#### REDUCTION OF METAL OXIDES IN AN ELECTROLYTIC CELL

The present invention relates to reduction of metal oxides in an electrolytic cell.

5

The present invention was made during the course of an on-going research project on the electrolytic reduction of titania (TiO<sub>2</sub>) carried out by the applicant.

During the course of the research project the applicant carried out experimental work on an electrolytic cell that included a graphite crucible that formed an anode of the cell, a pool of molten CaCl2-based electrolyte in the crucible, and a cathode that included solid titania.

One objective of the experimental work was to reproduce the results reported in International application PCT/GB99/01781 (Publication no. WO99/64638) in the name of Cambridge University Technical Services Limited and in technical papers published by the inventors.

The Cambridge International application discloses two potential applications of a "discovery" in the field of metallurgical electrochemistry.

One application is the direct production of a metal from a metal oxide.

30

35

20

In the context of this application, the "discovery" is the realisation that an electrolytic cell can be used to ionise oxygen contained in a metal oxide so that the oxygen dissolves in an electrolyte. The Cambridge International application discloses that when a suitable potential is applied to an electrolytic cell with a metal oxide as a cathode, a reaction occurs whereby

- 2 -

oxygen is ionised and is subsequently able to dissolve in the electrolyte of the cell.

European patent application 9995507.1 derived from the Cambridge International application has been allowed by the European Patent Office.

10

The allowed claims of the European patent application inter alia define a method of electrolytically reducing a metal oxide (such as titania) that includes operating an electrolytic cell at a potential that is lower than the deposition potential of cations in the electrolyte.

15 The Cambridge European patent application does not define what is meant by deposition potential and does not include any specific examples that provide values of the deposition potential for particular cations.

However, submissions dated 2 October 2001 to the European Patent Office by the Cambridge patent attorneys, which pre-dated the lodgement of the claims that were ultimately allowed, indicate that they believe that the decomposition potential of an electrolyte is the deposition potential of a cation in the electrolyte.

Specifically, page 5 of the submissions state that:

The second advantage described above is achieved in part through carrying out the claimed invention below the decomposition potential of the electrolyte. If higher potentials are used then, as noted in D1 and D2, the cation in the electrolyte deposits on the metal or semi
metal compound. In the example of D1, this leads to calcium deposition and therefore consumption of this reactive metal..........During operation of the method, the

- 3 -

electrolytic cation is not deposited on the cathode".

Contrary to the findings of Cambridge, the experimental work carried out by the applicant has established that it is essential that the electrolytic cell be operated at a potential that is above the potential at which Ca<sup>++</sup> cations in the electrolyte can deposit as Ca metal on the cathode.

5

30

10 Specifically, as a consequence of the experimental work, the applicant has invented a method of reducing a metal oxide such as titanium oxides in a solid state in an electrolytic cell which includes an anode, a cathode formed at least in part from the metal oxide, and 15 a molten electrolyte which includes cations of a metal that is capable of chemically reducing the cathode metal oxide, which method includes a step of operating the cell at a potential that is above a potential at which cations of the metal that is capable of chemically reducing the cathode metal oxide deposit as the metal on the cathode, 20 whereby the metal chemically reduces the cathode metal oxide.

The above method is described in Australian provisional application PS3049 in the name of the applicant lodged on 20 June 2002, and the disclosure in the patent specification lodged with the application is incorporated herein by cross-reference.

In addition to the above, the experimental work (and associated theoretical analysis work) carried out by the applicant has determined a number of important factors that play a role in the actual reduction process.

35 The relevant experimental data indicates that (i) Cl<sub>2</sub> gas is removed at the anode of the electrolytic cell at potentials well below the theoretical decomposition

- 4 -

potential of the electrolyte  $CaCl_2$ , (ii)  $Ca_XTi_YO_Z$ , is present at the cathode during some stages of the electrolysis, and (iii) CaO is formed in the molten electrolyte bath.

5

In view of the above, the applicant has concluded that a number of steps are involved in the method of reducing titanium oxides and that some of these steps are represented by reactions (1) to (8) mentioned below.

- Reactions (1) to (8) relate to reduction of titanium oxides using an electrolytic cell with CaCl<sub>2</sub> (containing O anions) as the electrolyte and a graphite anode, with their standard potentials at 950°C.
- 15  $CaCl_2 + 3TiO_2 = CaTiO_3 + Cl_2(g) + Ti_2O_3$  ...(1)  $E^{\circ}_{950C} = -1.45 \text{ V}$ 
  - $CaCl_2 + 2TiO_2 = CaTiO_3 + Cl_2(g) + TiO$  ... (2)  $E^{\circ}_{950C} = -1.63 \text{ V}$

20

$$CaCl_2 + 0.5TiO_2 = CaO + Cl_2(g) + 0.5Ti$$
 ... (3)  
 $E^{\circ}_{950C} = -2.4 \text{ V}$ 

$$CaTiO_3 + C = CaO + TiO + CO(g)$$
 ... (4)

 $25 E^{\circ}_{950C} = -0.86 V$ 

CaTiO<sub>3</sub> + 2C = CaO + Ti + 2CO(g) ... (5)  

$$E^{\circ}_{950C} = -0.96 \text{ V}$$

30 
$$Ti_2O_3 + C = 2TiO + CO(g)$$
 ... (6)  $E^{\circ}_{950C} = -0.58 \text{ V}$ 

TiO + C = Ti + CO(g) ... (7)  

$$E^{\circ}_{950C} = -1.07 \text{ V}$$

35

$$[0] Ti + C = CO(gas) \qquad ... (8)$$

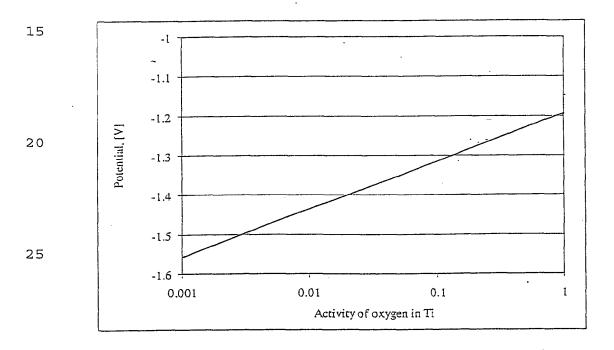
~ 5 -

Reactions (1) to (8) are not an exhaustive list, of the possible reaction and other reactions can take place. Specifically, the applicant suspects that other reactions, involving titanium suboxides, represented by the formula  ${\rm Ti_nO_{2n-1}}$ , and calcium titanates, represented by the formula  ${\rm CaTi_nO_{3n+1}}$ , can take place.

The potential of reaction (8) in particular varies with the concentration of oxygen in titanium. The following graph illustrates the variation of potential with concentration of oxygen in titanium in a cell operating at 950°C. The graph was prepared by the applicant using published data.

10

30



It is clear from the graph that reaction (8) requires higher potentials at lower concentrations of oxygen and thus there is increased resistance to oxygen removal as the oxygen concentration decreases.

35 The solubility of different titanium oxides in CaCl<sub>2</sub> is not taken into consideration in the calculation of the potentials for reactions (1) to (8). The significance

- 6 -

of this is that some of reactions (1) to (8) may take place at potentials that are higher or lower than the potentials stated above at the stated temperature of 950°C.

For example, reduced activity of TiO will reduce the value of the potentials of reactions (2), (4) and (6) (i.e. make the potentials more positive) and at the same time will increase the potential of reaction (7) (i.e. make it more negative).

10

15

20

5

In view of the above, the applicant has realised that it is likely to be extremely difficult to reduce titanium oxide in an electrolytic cell to titanium ( $\alpha$ Ti) of high purity, i.e. low concentration of oxygen (no more than 100ppm oxygen) in a single stage operation.

Specifically, the applicant has realised that it is necessary to refresh the electrolyte and/or to change cell potential in a later stage or in later stages of the operation of the electrolytic cell in order to reduce titanium oxide in an electrolytic cell to  $\alpha$  titanium of high purity, ie low concentration of oxygen.

According to the present invention there is provided a method of reducing a titanium oxide in a solid 25 state in an electrolytic cell which includes an anode, a cathode formed at least in part from the titanium oxide, and a molten electrolyte which includes cations of a metal that is capable of chemically reducing the cathode 30 titanium oxide, which method includes operating the cell at a potential that is above a potential at which cations of the metal that is capable of chemically reducing the cathode titanium oxide deposit as the metal on the cathode, whereby the metal chemically reduces the cathode titanium oxide, and which method is characterised by 35 refreshing the electrolyte and/or changing the cell potential in later stages of the operation of the cell as

- 7 -

required having regard to the reactions occurring in the cell and the concentration of oxygen in the titanium oxides in the cell in order to produce high purity titanium ( $\alpha$ Ti).

5

The term "high purity" is understood to mean that the concentration of oxygen is no more than 100ppm in the titanium.

In effect, the present invention is concerned

with selecting the operating conditions of the cell,
including cell potential and/or electrolyte composition,
during various stages of the operation in the cell having
regard to the reactions that take place in the cell. The
applicant envisages at this stage that commercial

operations will be at constant currant and that it may not
be possible to achieve voltages required to remove oxygen
to very low levels because of composition changes in the
electrolyte. In these circumstances, refreshing and or
changing the electrolyte composition is important in order
to produce a high purity α titanium.

The above-described method makes it possible to produce titanium of high purity with respect to oxygen in an electrolytic cell and without refining or otherwise processing the titanium outside the electrolytic cell.

The method may include refreshing the electrolyte by adding new electrolyte to the existing electrolyte or otherwise adjusting the composition of the electrolyte.

30

25

In addition, the method may include carrying out the method in a series of electrolytic cell and successively transferring the partially reduced titanium oxide to each of the cells in the series.

35

The composition of the electrolyte in each cell may be selected having regard to the reactions occurring

- 8 -

in the cell and the concentration of oxygen in the titanium oxide in the cell.

The cell potential may be changed at different stages in the method on a continuous or a step-change basis.

Preferably the metal deposited on the cathode is soluble in the electrolyte and can dissolve in the electrolyte and thereby migrate to the vicinity of the cathode titanium oxide.

It is preferred that the electrolyte be a CaCl<sub>2</sub>-based electrolyte that includes CaO as one of the constituents of the electrolyte.

In such a situation it is preferred that the cell potential be above the potential at which Ca metal can deposit on the cathode, i.e. the decomposition potential of CaO.

2.0

25

30

The decomposition potential of CaO can vary over a considerable range depending on factors such as the composition of the anode, the electrolyte temperature and electrolyte composition.

In a cell containing CaO saturated  $CaCl_2$  at 1373K (1100°C) and a graphite anode this would require a minimum cell potential of 1.34V.

It is also preferred that the cell potential be below the decomposition potential of  $CaCl_2$ .

In a cell containing CaO saturated CaCl<sub>2</sub> at 1373K (1100°C) and a graphite anode this would require that the cell potential be less than 3.5V.

- 9 -

The decomposition potential of  $CaCl_2$  can vary over a considerable range depending on factors such as the composition of the anode, the electrolyte temperature and electrolyte composition.

5

For example, a salt containing 80% CaCl<sub>2</sub> and 20% KCl at a temperature of 900% (657°C), decomposes to Ca (metal) and Cl<sub>2</sub> (gas) above 3.4V and a salt containing 100% CaCl<sub>2</sub> at 1373% (1100°C) decomposes at 3.0%.

10

In general terms, in a cell containing  $CaO-CaCl_2$  salt (not saturated) at a temperature in the range of 600-1100°C and a graphite anode it is preferred that the cell potential be between 1.3 and 3.5V.

15

The CaCl<sub>2</sub>-based electrolyte may be a commercially available source of CaCl<sub>2</sub>, such as calcium chloride dihydrate, that partially decomposes on heating and produces CaO or otherwise includes CaO.

20

Alternatively, or in addition, the CaCl<sub>2</sub>-based electrolyte may include CaCl<sub>2</sub> and CaO that are added separately or pre-mixed to form the electrolyte.

25

30

It is preferred that the anode be graphite or an inert anode.

The cell may be of the type disclosed in the drawings of the patent specification lodged with Australian provisional application PS3049.

- 10 -

CLAIMS

WO 03/002785

A method of reducing a titanium oxide in a solid state in an electrolytic cell which includes an anode, a cathode formed at least in part from the titanium oxide, and a molten electrolyte which includes cations of a metal that is capable of chemically reducing the cathode titanium oxide, which method includes operating the cell at a potential that is above a potential at which cations of the metal that is capable of chemically reducing the 10 cathode titanium oxide deposit as the metal on the cathode, whereby the metal chemically reduces the cathode titanium oxide, and which method is characterised by refreshing the electrolyte and/or changing the cell potential in later stages of the operation of the cell as 15 required having regard to the reactions occurring in the cell and the concentration of oxygen in the titanium oxides in the cell in order to produce high purity titanium (aTi).

PCT/AU02/00843

20

2. The method defined in claim 1 wherein the metal deposited on the cathode is soluble in the electrolyte and can dissolve in the electrolyte and thereby migrate to the vicinity of the cathode titanium oxide.

25

- 3. The method defined in claim 1 or claim 2 wherein the electrolyte is a  $CaCl_2$ -based electrolyte that includes CaO as one of the constituents of the electrolyte.
- 30 4. The method defined in claim 3 wherein the cell potential be above the potential at which Ca metal can deposit on the cathode, i.e. the decomposition potential of CaO.
- 35 5. The method defined in claim 3 or claim 4 wherein the cell potential is below the decomposition potential of CaCl<sub>2</sub>.

- 11 -

6. The method defined in any one of claims 3 to 5 wherein at a temperature in the range of 600-1100°C and a graphite anode the cell potential is between 1.3 and 3.5V.

5

10

15

- 7. The method defined in any one of claims 3 to 6 wherein the CaCl<sub>2</sub>-based electrolyte is a commercially available source of CaCl<sub>2</sub>, such as calcium chloride dihydrate, that partially decomposes on heating and produces CaO or otherwise includes CaO.
- 8. The method defined in any one of claims 3 to 7 wherein the CaCl<sub>2</sub>-based electrolyte includes CaCl<sub>2</sub> and CaO that are added separately or pre-mixed to form the electrolyte.
- 9. The method defined in any one of the preceding claims wherein the anode is graphite or an inert anode.

## INTERNATIONAL SEARCH REPORT

International application No.

## PCT/AU02/00843

A.	CLASSIFICATION OF SUBJECT MATTER						
Int. Cl. 7;	C25C 3/28, C22B 34/12						
According to	o International Patent Classification (IPC) or to both	national classification and IPC	_				
В.	FIELDS SEARCHED	-					
	cumentation searched (classification system followed by classification sys	assification symbols)					
	C 3/28, C22B 34/12						
Documentatio	on searched other than minimum documentation to the exte	nt that such documents are included in the fields searc	hed				
	ta base consulted during the international search (name of CECTROLYT+	data base and, where practicable, search terms used)					
C.	DOCUMENTS CONSIDERED TO BE RELEVANT						
Category*	Citation of document, with indication, where appr	copriate, of the relevant passages	Relevant to claim No.				
	WO 99/64638 A (CAMBRIDGE UNIVERSI	TY TECHNICAL SERVICES LTD)					
A	16 December 1999 whole document		1-9				
			1				
A	GB 2359564 A (THE SECRETARY OF STATE FOR DEFENCE) 29 August whole document						
1.	Whole document		1-9				
A	WO 01/62994 A (THE SECRETARY OF ST whole document	FATE FOR DEFENCE) 30 August 2001	1-9				
X	Further documents are listed in the continuation	of Box C X See patent family anne	ex				
* Special categories of cited documents:  "A" document defining the general state of the art which is not considered to be of particular relevance  "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention							
	he international filing date co	cument of particular relevance; the claimed invention nsidered novel or cannot be considered to involve an nen the document is taken alone					
claim(	nent which may throw doubts on priority "Y" do (s) or which is cited to establish the co	nsidered to involve an inventive step when the docum nsidered to involve an inventive step when the docum th one or more other such documents, such combination	ent is combined				
reason	son (as specified)  a person skilled in the art  document referring to an oral disclosure, use,  "&"  document member of the same patent family						
exhibi "P" docum	tion or other means nent published prior to the international filing ut later than the priority date claimed	•					
	tual completion of the international search	Date of mailing of the international search report					
27 August 2		5 SEP 2002					
	iling address of the ISA/AU	Authorized officer					
PO BOX 200, E-mail address	N PATENT OFFICE WODEN ACT 2606, AUSTRALIA s: pct@ipaustralia.gov.au	B. PREMARATNE					
Facsimile No.	(02) 6285 3929	Telephone No: (02) 6283 2407					

## INTERNATIONAL SEARCH REPORT

International application No.

## PCT/AU02/00843

C (Continuation). DOCUMENTS CONSIDERED TO BE RELEVANT						
Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.				
A	US 4518426 A (MURPHY) 21 May 1985 whole document	1-9				
A	US 4381976 A (ARMAND) 3 May 1983 whole document	1-9				

#### INTERNATIONAL SEARCH REPORT

Information on patent family members

International application No.

PCT/AU02/00843

This Annex lists the known "A" publication level patent family members relating to the patent documents cited in the above-mentioned international search report. The Australian Patent Office is in no way liable for these particulars which are merely given for the purpose of information.

Patent Document Cited in Search Report		Patent Family Member					
WO	9964638	AU	42770/99	BR	9910939	CZ	20004476
		EP	1088113	$\mathbf{H}\mathbf{U}$	200102934	NO	20006154
		PL	344678				
GB	2359564	AU	200133871	AU	200133876	AU	200133890
		wo	200162994	WO	200162995	WO	200162996
		GB	2362164				
US	4518426	US	4487677	AU	27774/84	CA	1261297
US	4381976	EP	53566	FR	2494726	JР	57116791
		NO	814030				
	1						END OF ANNEX